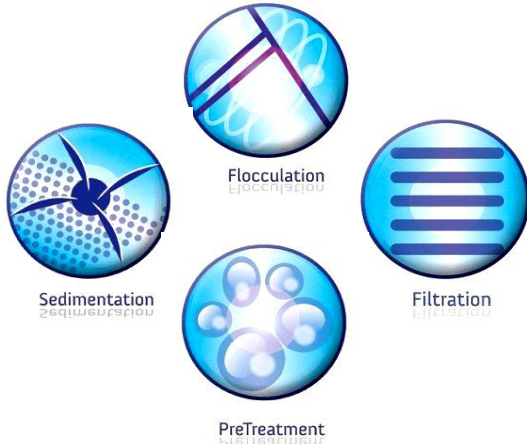


October 17th, 2017



## Development and Scale-up of Cell Culture Harvest Processes for Biopharmaceutical Production

BioProduction Conference 2017  
Convention Centre Dublin, Ireland



**Markus Brakel**  
Boehringer Ingelheim Pharma  
Biopharmaceuticals Germany  
BPAD Cell Culture CMB



# Boehringer Ingelheim BioXcellence™

## World-wide customer orientation



# Boehringer Ingelheim Biopharmaceuticals Production Network

## Microbial & Yeast

Mammalian...soon

Vienna, Austria



Commercial capacity for  
microbials and yeast  
fermentation products

Biberach, Germany



Commercial capacity  
for cell culture  
products

## Mammalian

Fremont, USA



Commercial capacity  
for cell culture  
products

Shanghai, China



Commercial capacity for  
cell culture products  
Disposable Technology

Vienna, Austria



Fermentation Capacity:  
F1: 30 L, 300 L, 6,000 L  
F2: 30 L, 300 L, 6,000 L

Biberach, Germany



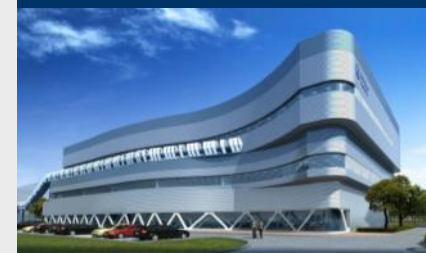
Fermentation Capacity:  
16x 15,000 L Bioreactors  
12x 2,000 L Bioreactors

Fremont, USA



Fermentation Capacity:  
2 x 15,000 L Bioreactors  
4 x 2,000 L Bioreactors

Shanghai, China

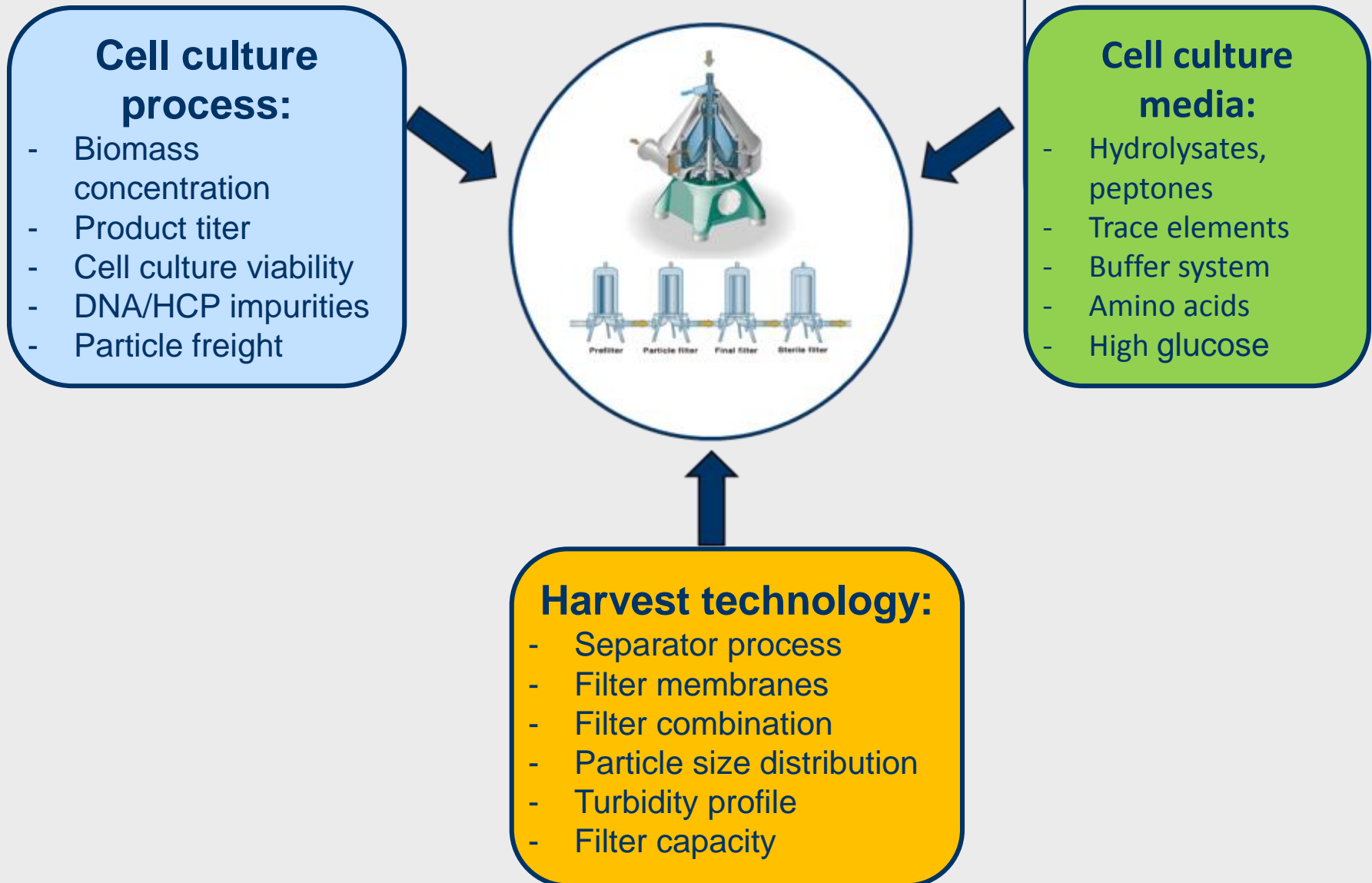


Fermentation Capacity:  
1x 2,000 L SUB bioreactors  
2x 500 L SUB bioreactors



# BI's Cell Culture Harvest Processes

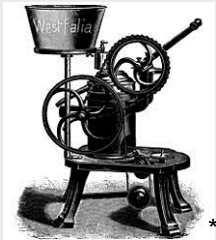
## Challenges for separation and filtration



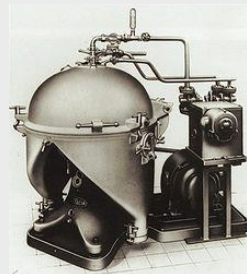
# BI's Cell Culture Harvest Processes

## History of centrifugation and filtration

1893



1931



1985



1995...



Milk - buttermilk – cream – butter  
Food and beverage (beer, fruit juice)

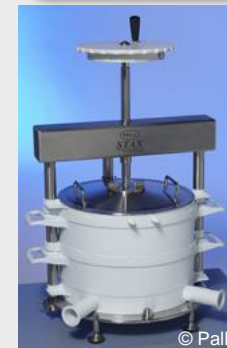
Centrifugation and  
filtration in modern  
Biotechnology



Hollow fibre  
Filter discs

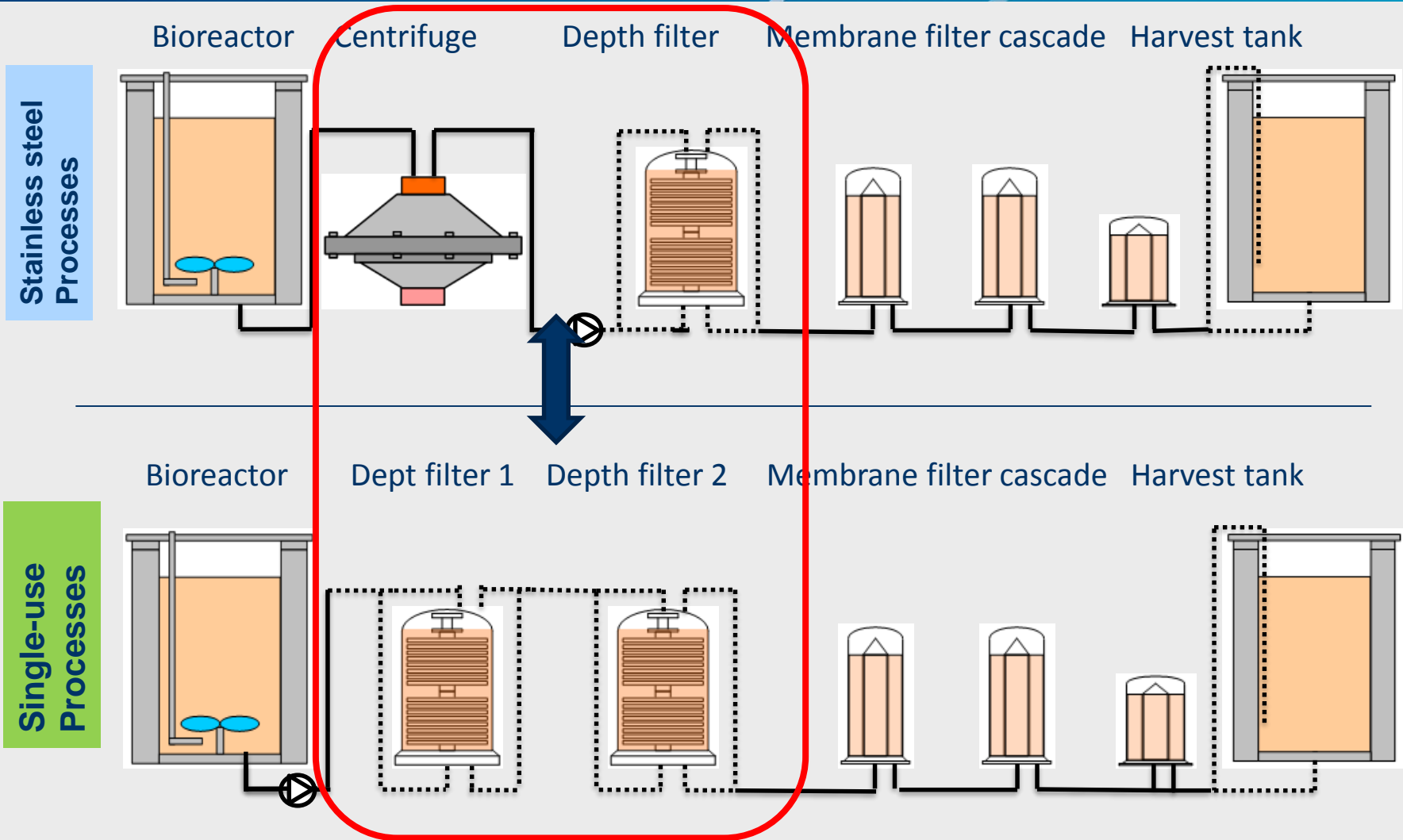


TFF Filters



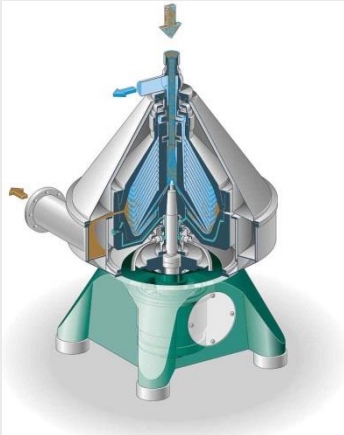
# BI's Cell Culture Harvest Processes

## Stainless steel vs. Single-use processes



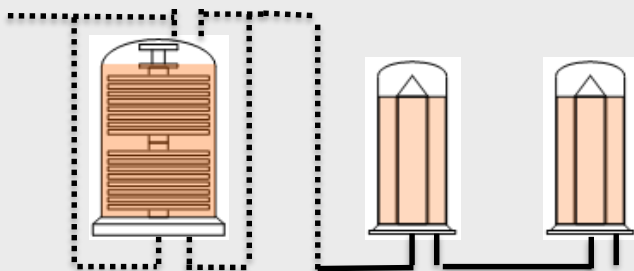
## Separation and filtration

### Centrifugation / Separation



- Gravimetric clarification of cell culture
- Reduction of biomass and turbidity
- Continuous desludging disc stack separator
- Key parameters: Biomass (PCV%)  
Feed flow rate  $Q$   
Depletion time  $T$   
Inlet/outlet pressure  $P$   
Equivalent clearance area  $\Sigma$
- Scale up criteria:  $Q/\Sigma = \text{const.}$

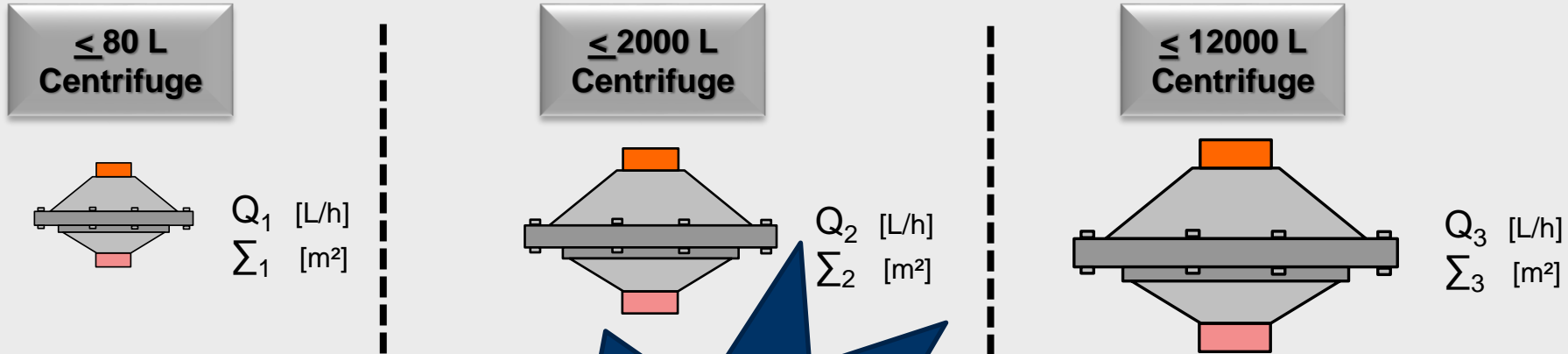
### Depth- and Membrane filtration



- Mechanical reduction of particles
- Reduction of PRI: DNA, HCP, cell debris, particles
- Key parameters: Filter types and combination  
Filter material characteristics  
Filtration flow rate and flux rate  
Total filter area
- Scale up criteria: Filter types and combin. = const.  
Flux rate = constant  $[\text{L}/\text{m}^2\text{h}]$   
Max. filter capacity = const.  $[\text{L}/\text{m}^2]$

# BI's Cell Culture Harvest Processes

## Scale up of Separation processes



$$\frac{Q}{\Sigma} = \frac{2\pi}{3g} \cdot \omega^2 \cdot r \cdot \alpha \cdot N \cdot \cos^3(\alpha) = \text{Const.}$$

**Experience & Know-How is essential**

Scale up factors:  
 $Q$  = feed flow rate of centrifuge [ L/h ]  
 $\Sigma$  = equivalent clearance area [ m<sup>2</sup> ]  
 $Q/\Sigma = \text{const.}$

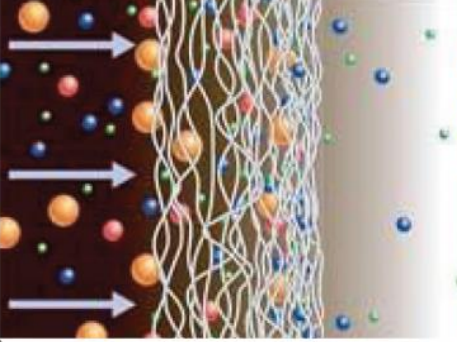
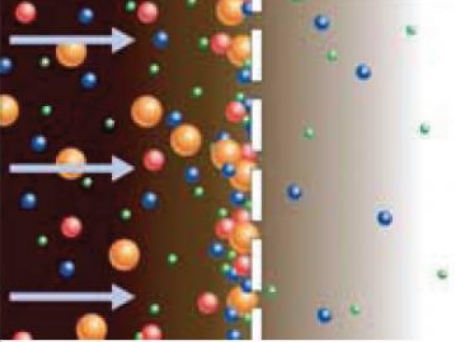
Separator characteristics:  
 $\omega$  = rotational velocity  
 $N$  = number of discs  
 $\alpha$  = the conical half angel  
 $r_1$  = inner radius of disc  
 $r_2$  = outer radius of disc

Process parameters:  
 Inlet/outlet pressure  
 Depletion strategy  
 Feed flow rate  
 Rotation speed [rpm]  
 G-force [m/s<sup>2</sup>]



# BI's Cell Culture Harvest Processes

## Filtration development & scale up

	Depth filtration	Membrane filtration
		
Principle	Particles trapped in filter depth	Particles stopped on filter surface
Filtration media	Deep filtration media	Thin filtration media
Applications	<ul style="list-style-type: none"> <li>- Filtration of larger suspended solids</li> <li>- Large or undefined particle sizes</li> <li>- Prefiltration</li> </ul>	<ul style="list-style-type: none"> <li>- Filtration of finer suspended solids</li> <li>- Narrow or defined particle sizes</li> <li>- Prefiltration and final filtration</li> </ul>
Cost	Low (disposable after use)	High (cleanable with hot water or chemicals)
Type of cartridges	Wound and meltblown cartridges	Pleated cartridges

[www.pentairaquaeurope.com](http://www.pentairaquaeurope.com)

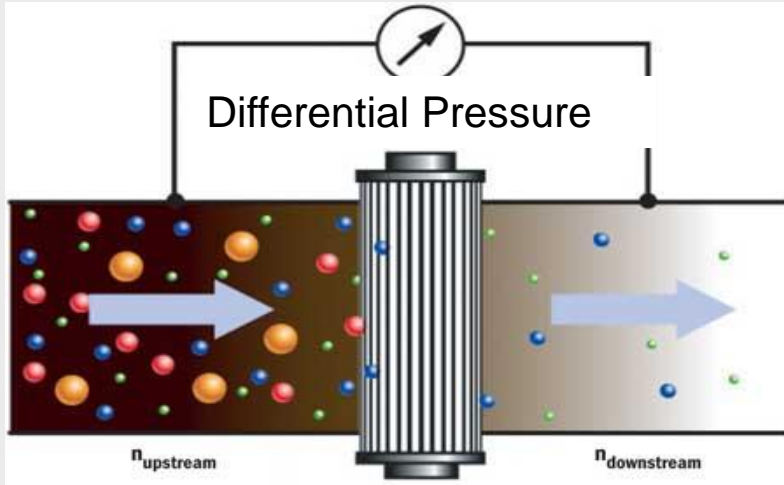
### Filter characteristics:

- Filter materials: PES, PTFE, Polypropylene, Polyethylene, Cellulose
- Hydrophilic / hydrophobic / charged / coated
- Filter design and „architecture“: hollow fibre, sheet, plate, column
- Porosity, Pore size distribution, pore symmetry
- Filter size and total membrane area

# BI's Cell Culture Harvest Processes

## Filtration development and scale-up

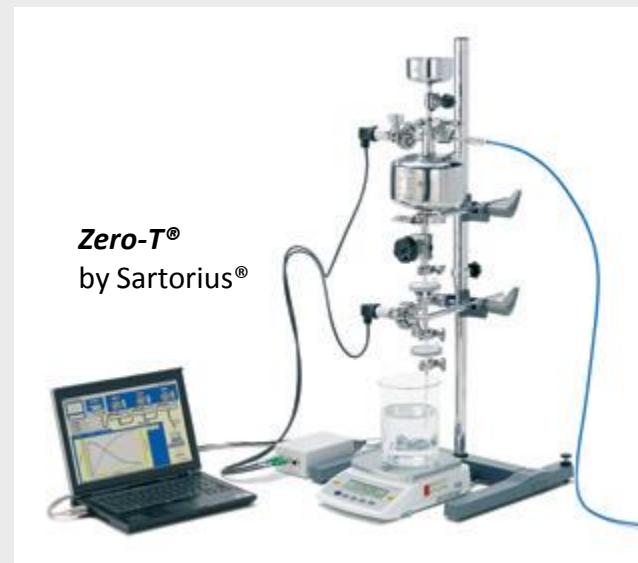
www.pentairaquaeurope.com



- Linear filter scale-down 12kL → 80L
- $P_{max}$  studies at constant flow rates
- Differential pressure profile analysis ( $P_{max}$ )
- Maximum filter capacity analysis ( $C_{max}$ )
- Particle-size-distribution analysis
- Turbidity trending analysis
- Calculation of product step yields
- Impurity reduction analysis (DNA, HCP)
- Small scale filtration studies and SDM dev.

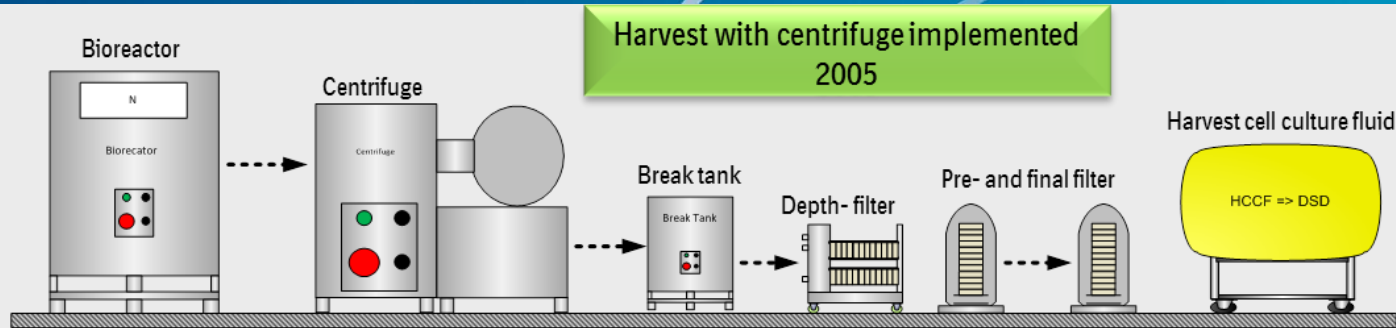
### Scale up strategy:

- Identical filter types
- Filter flux LMH [ $L/m^2h$ ] = const.
- $C_{max}$  at  $P_{max}$
- Linear scale up 80L → 2kL → 12kL



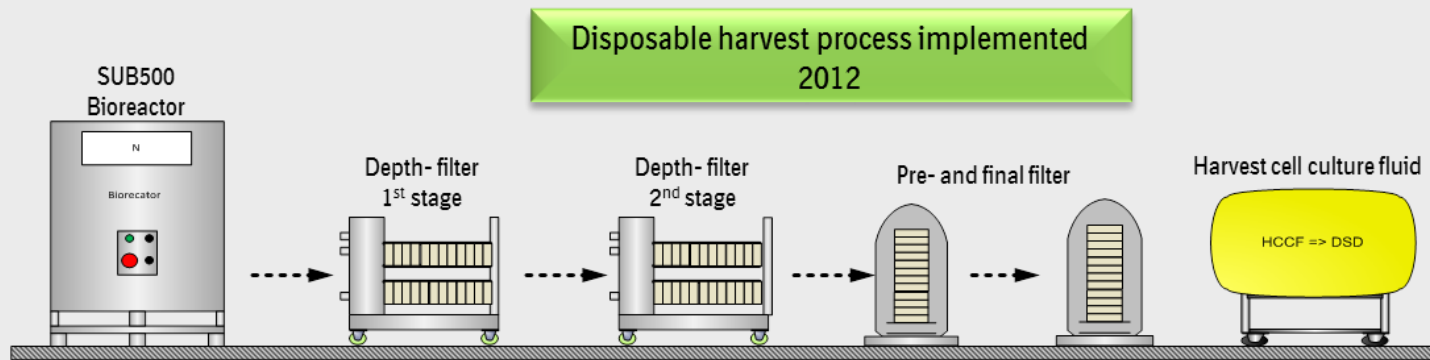
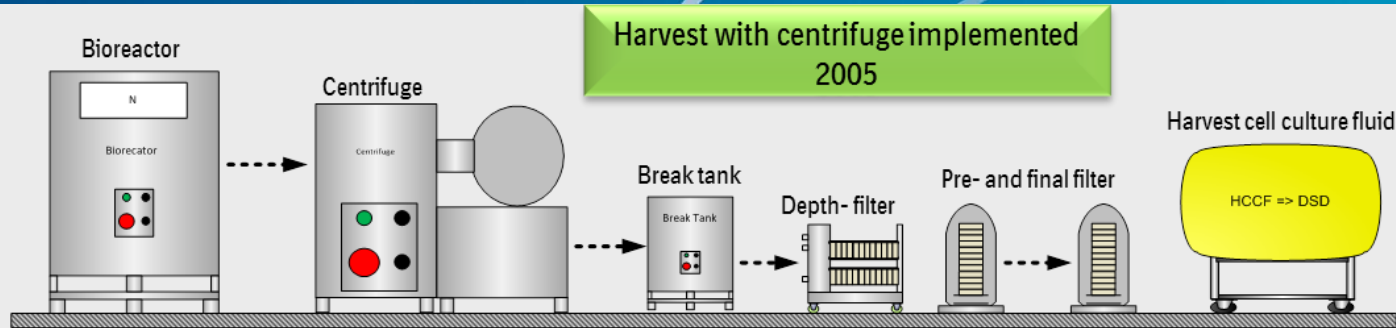
# BI's Cell Culture Harvest Processes

## Current Technology Status



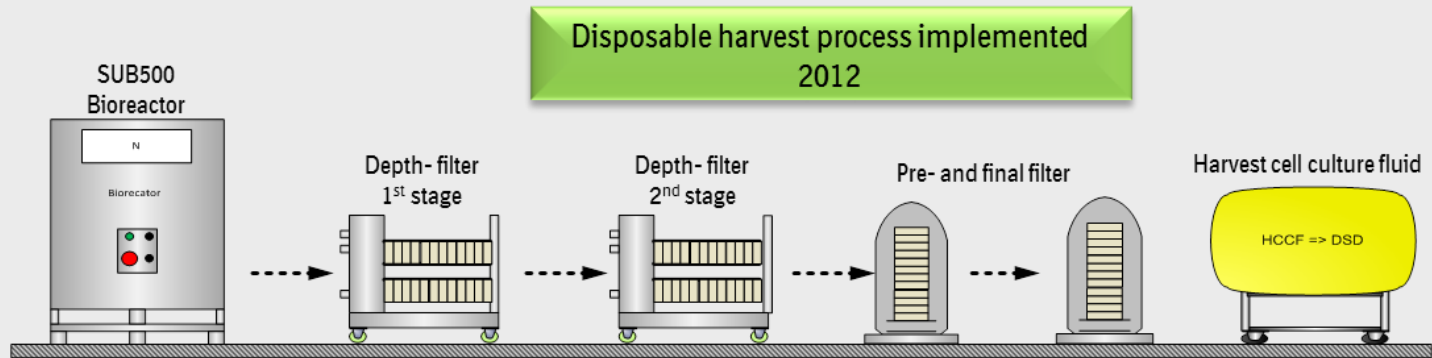
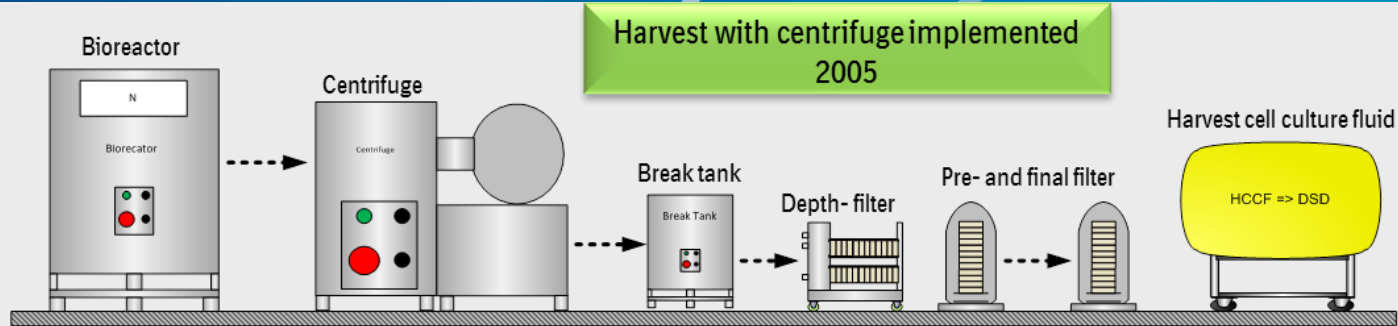
# BI's Cell Culture Harvest Processes

## Current Technology Status



# BI's Cell Culture Harvest Processes

## Current Technology Status



**Boehringer harvest development activities:**

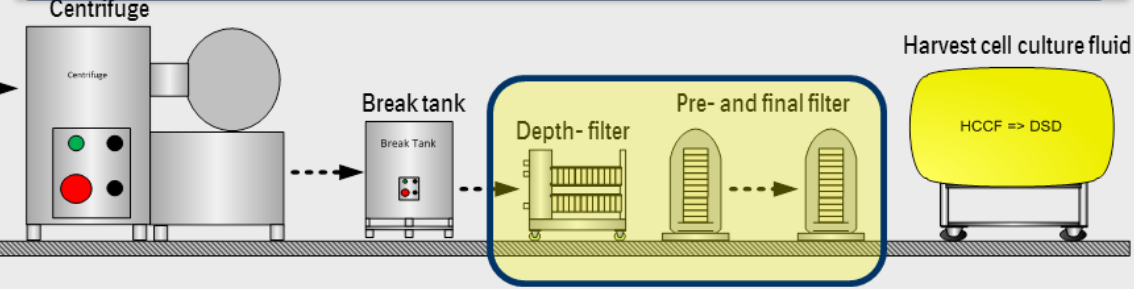
- Cell culture pre-treatment strategies
- New depth- and membrane filters

**Acid precipitation**

**Flocculation**

**Diatomaceous Earth filtration**

**Bioreactor**





# Case studies...

## Case study I: Process scale up & optimization in 12kL

### **Background:**

- Cell Culture Process development and successful consolidation in 80L stainless steel at BI.
- Process transfer from 80L Development scale to 12.000L production scale.
- Standard transfer procedures and scale up criteria were used.

### **Situation:**

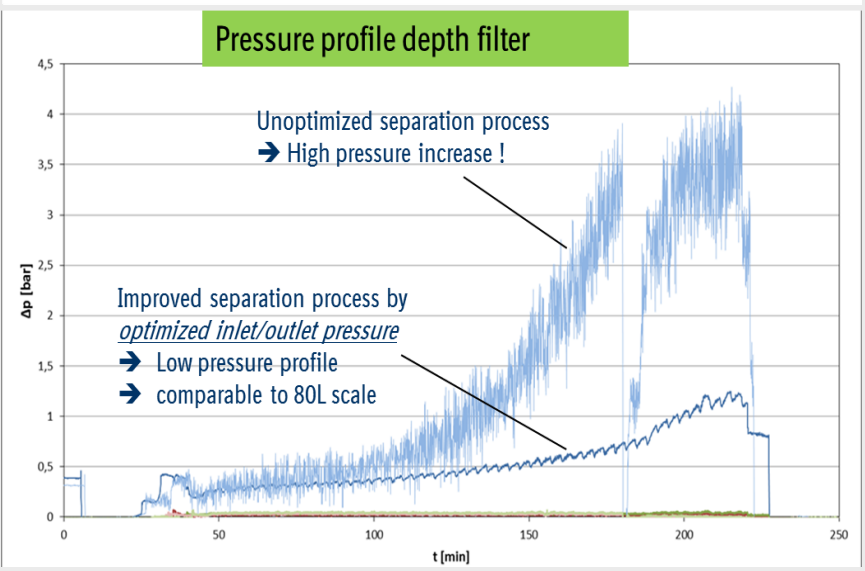
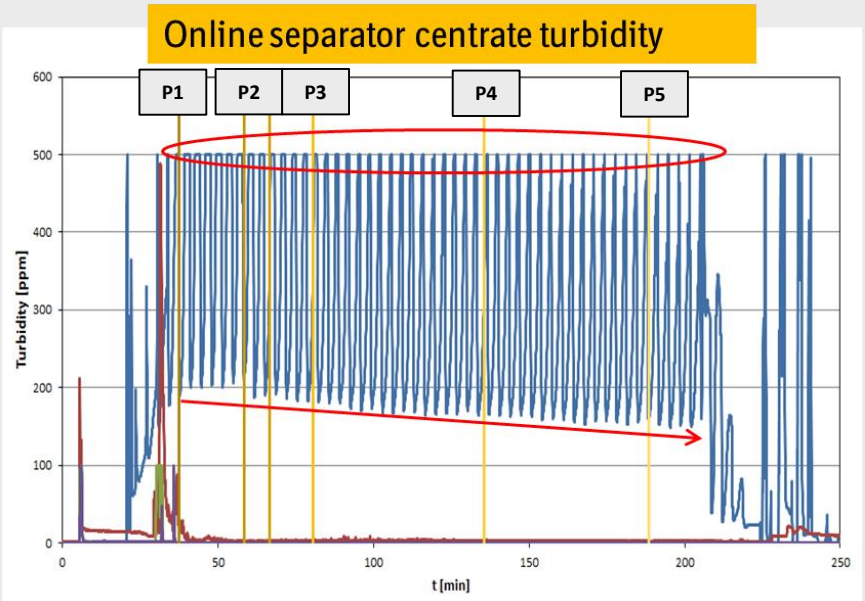
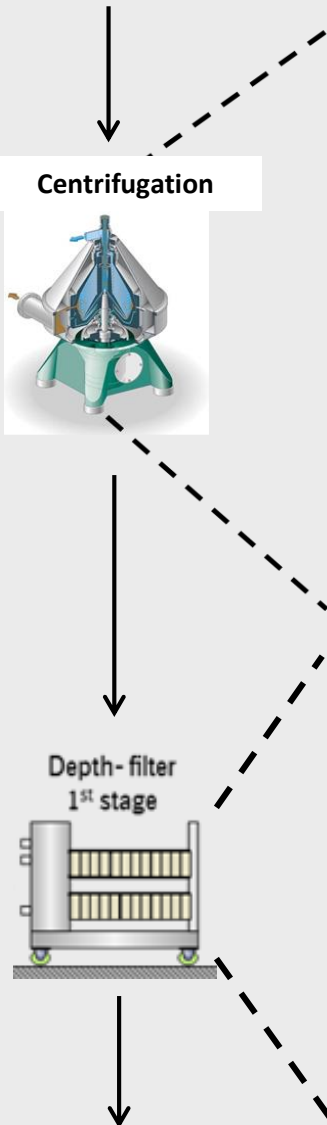
- First 12.000L large scale run showed a significant pressure increase on depth filters.
- Data analysis revealed an uncommon pattern of online turbidity profile in the centrifuge.
- Consultation of experts from development, operations and the supplier of the centrifuge.
- The inlet and outlet pressure in the separator was identified a key process parameter.
- The second process was performed using different pressure levels in the centrifuge.

### **Conclusion:**

- By the optimization of the inlet and outlet pressure of the centrifuge the clarification of biomass could be improved significantly .
- Finally, the process performance was very comparable to the 80L scale consolidation run.
- Successful process transfer and optimization by collaboration of technical experts from different departments.

# BI's Cell Culture Harvest Processes

## Case study I: Process scale up & optimization in 12kL



- Inlet and outlet pressure in centrifuge optimized at scale
- Inlet/outlet pressure influences concentrate turbidity after centrifuge
- Direct impact on clarification efficiency in separator
- Higher clarification efficiency improves particle freight on depth filters
- Lower pressure profile and higher filter capacities!
- Comparable performance 12.000L and 80L scale

### Background:

- Direct adaptation of 80L stainless steel into 500L SUB process in first run at BI
- Cell culture process with a high cell mass and a very high demand for glucose
- Initial harvest process using a two-stage depth filtration showed filter blocking
- Root cause: Cells show a high tendency for settling
- Filter blocking → very low product yield → optimization necessary ! FAST !

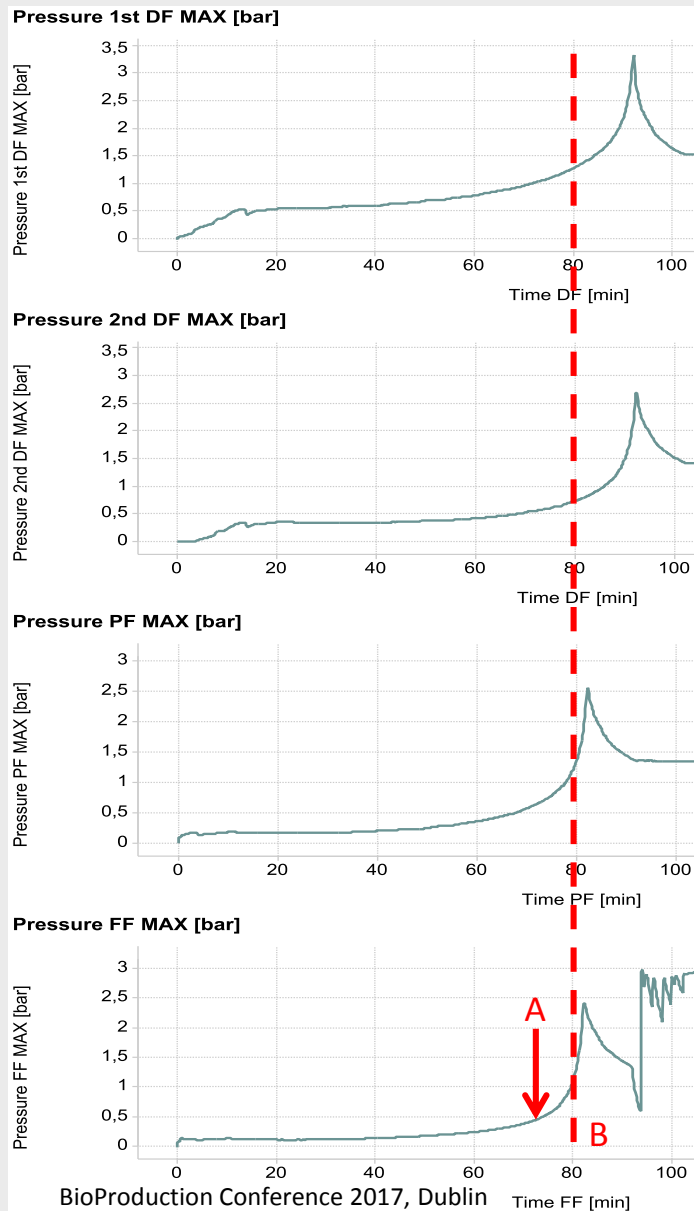
### Joint Harvest development:

- Collaboration with filter supplier for development of new depth filtration strategy
- BI: Introduction of a separate mixing tank in order to ensure good suspension
- Lab scale experiments in 2L - 80L scale by filter supplier at BI labs for testing filter options
- Successful implementation and scale up of new harvest strategy in 500L scale



# Cell Culture Harvest Processes Development

## Case Study II: Bringing Know-how together !



### **A:** Fast pressure increase

→ fast settling of solids (cells, debris etc.) to the bottom of the bioreactor!

→ Fast increase of solid particle concentration in filtration feed stream!

### **B:** Filter blockage

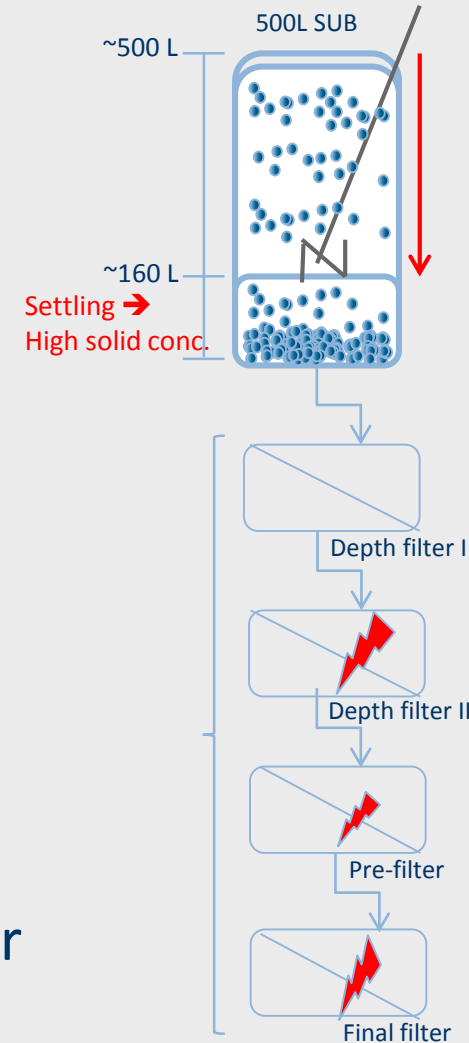
→ High concentration of solids at bottom

→ Rapid pressure increase in all filters

→ Insufficient particle clarification

→ Bottleneck in depth filter capacity!

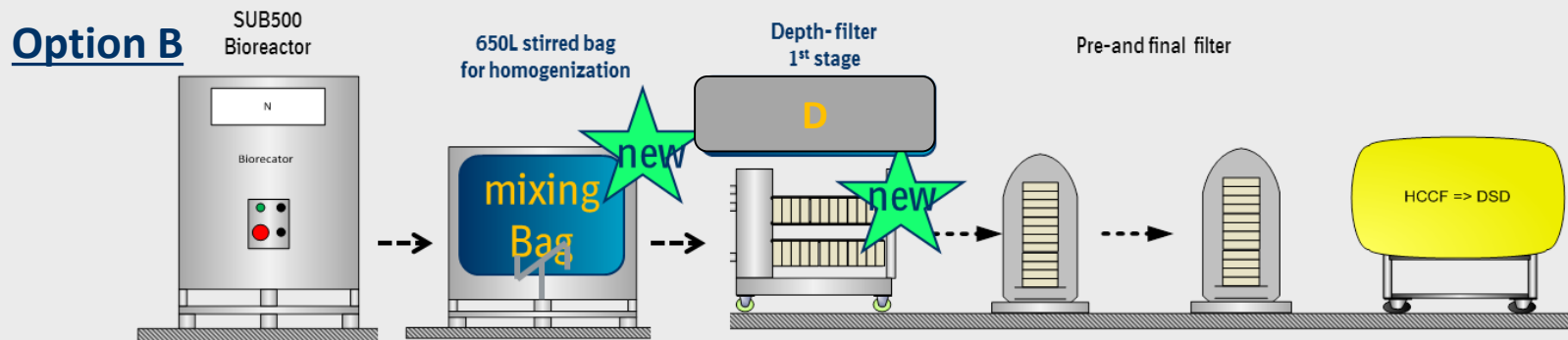
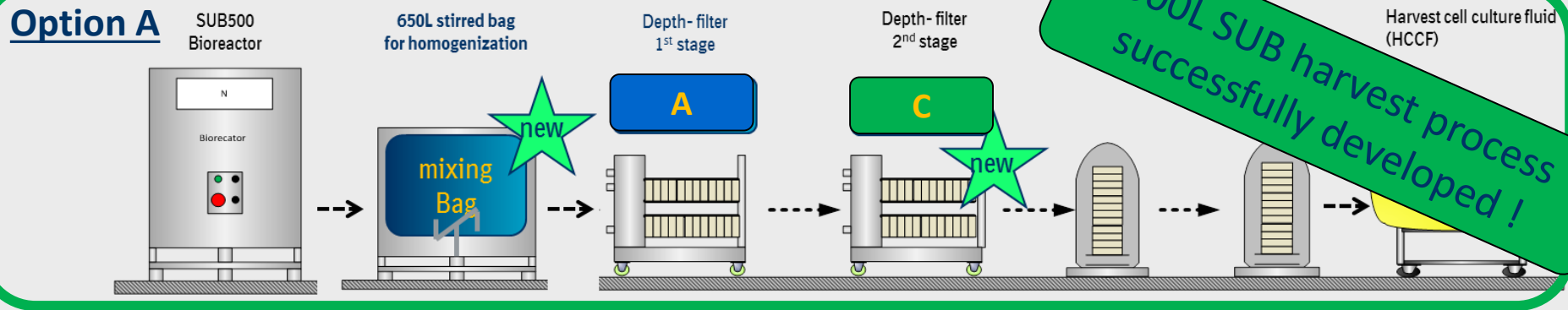
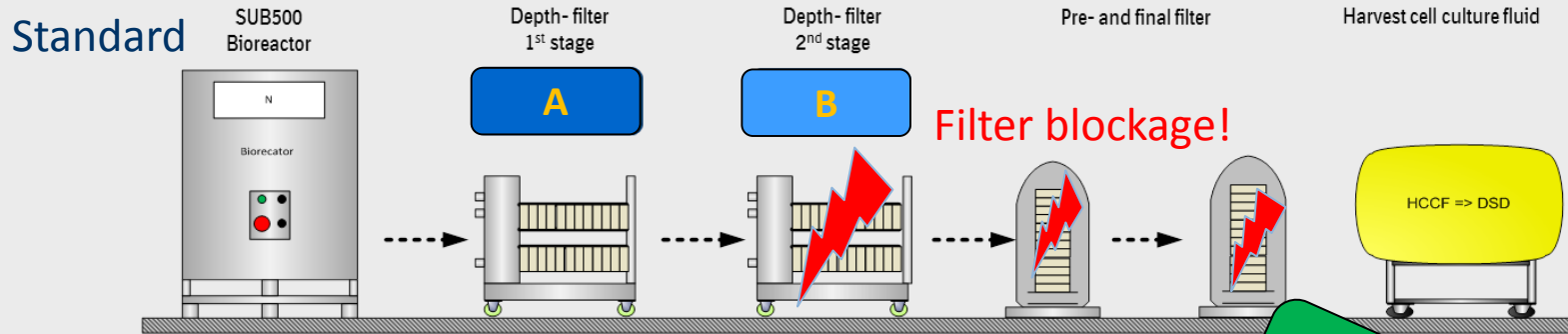
➔ Alternative depth filter needed!



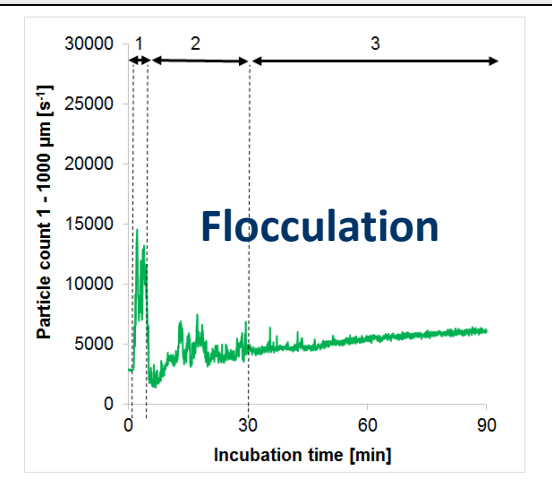
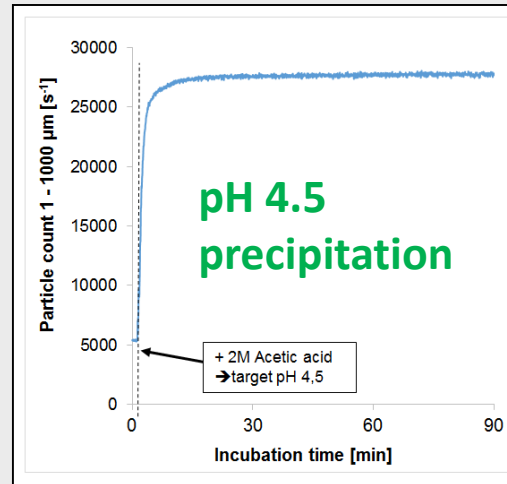
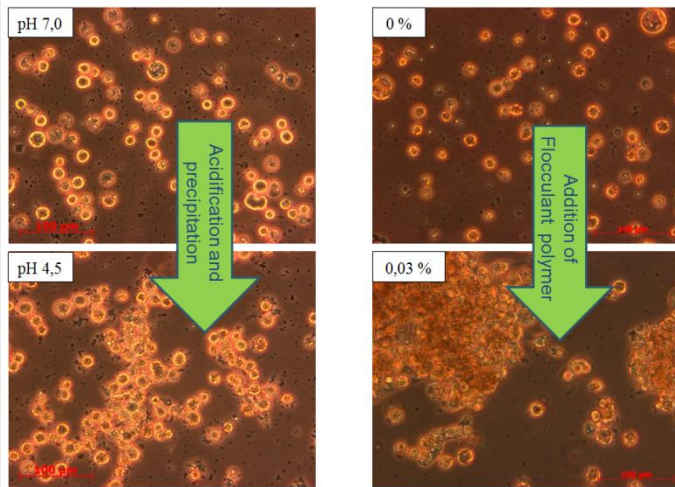
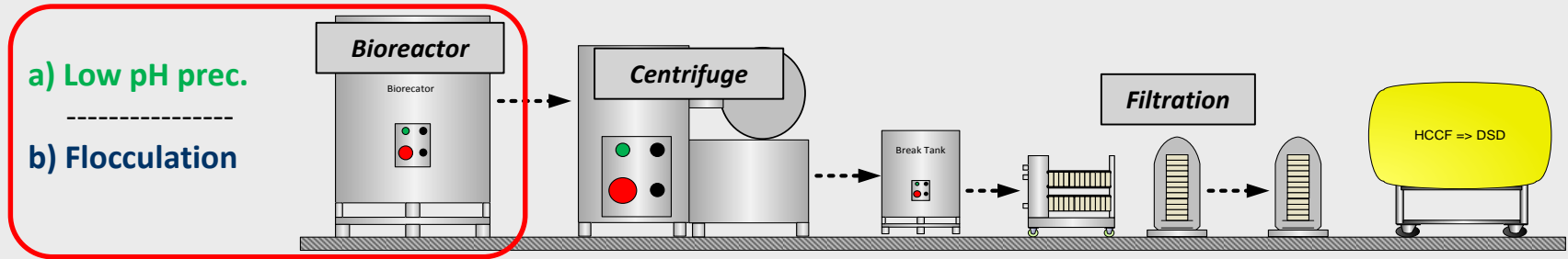


# Cell Culture Harvest Processes Development

## Case Study II: Bringing Know-how together !



## Case Study III: Pretreatment by precipitation vs. flocculation



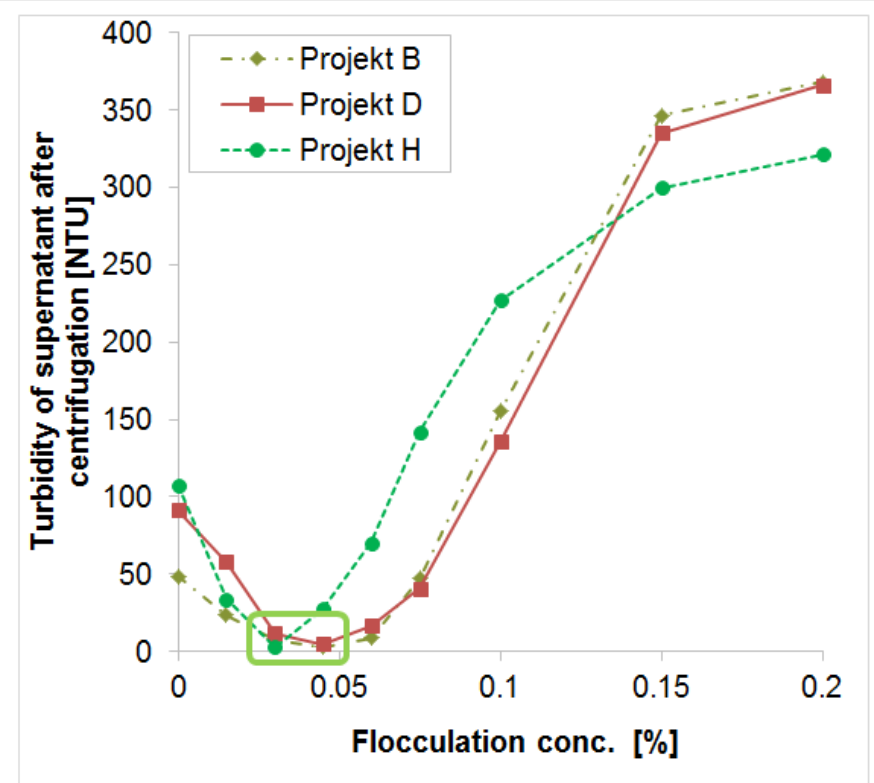
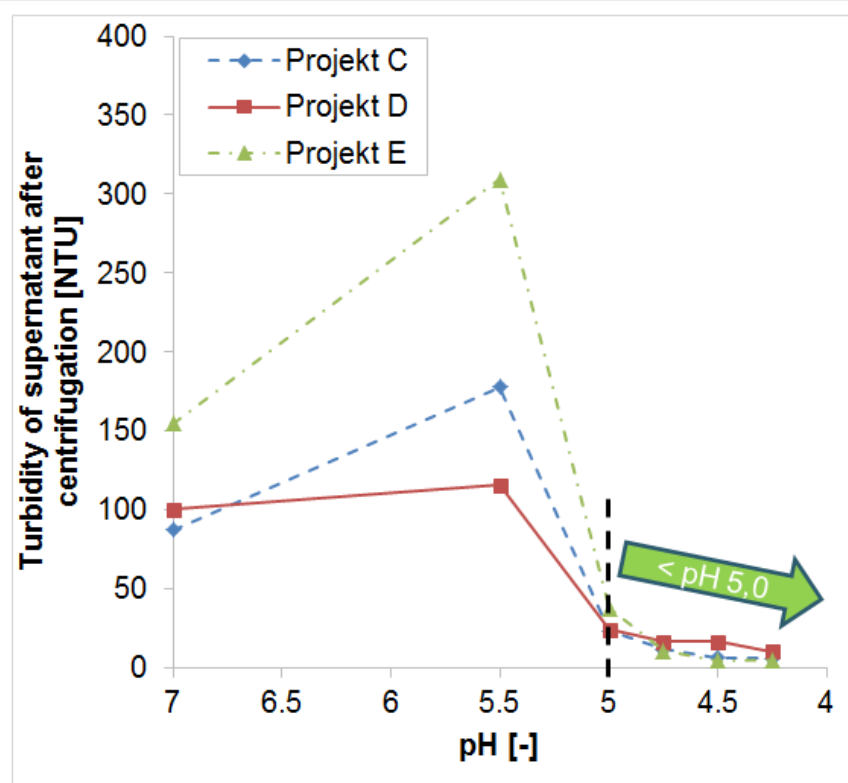
### Microscopic analysis:

- ➔ A direct low pH precipitation and flocculation in the cell culture have a different impact on particle formation and cell aggregation / cell lysis

### Online Particle size distribution analysis:

- ➔ Online FBRM probe (Mettler Toledo®)
- ➔ Precipitation/flocculation kinetics
- ➔ Low pH precipitation and flocculation have different particle formation kinetic

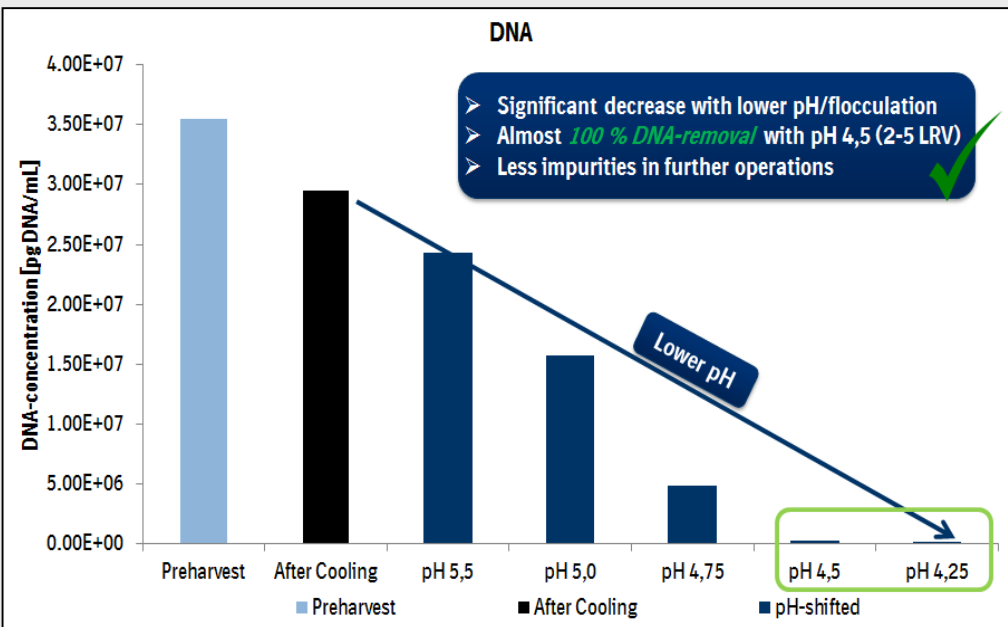
## Case Study III: Pretreatment by precipitation vs. flocculation



- Flocculation process with a small operational window (conc. range)
- Best precipitation results with low pH < 5.0 → Optimum: pH 4.5
- Flocculation process more challenging: polymer choice, concentration, incubation, analytics, removal of polymer during purification process

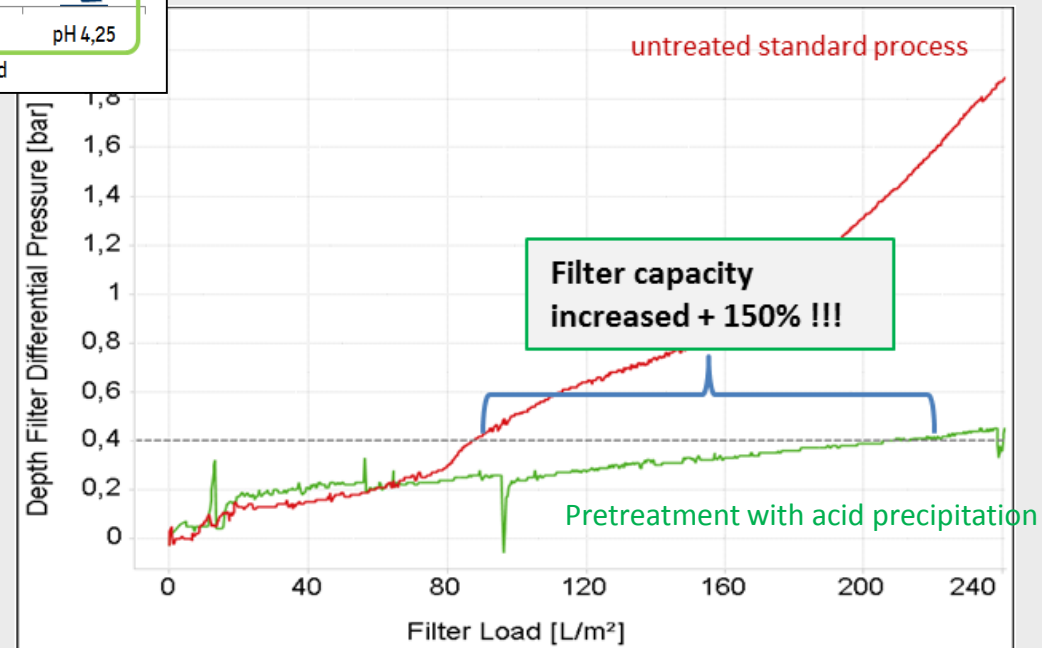
# BI's Cell Culture Harvest Processes

## Case Study III: Pretreatment by precipitation vs. flocculation



- > 99% DNA removal by low pH precipitation
- Optimal precipitation at pH 4.5
- Easy implementation in standard process

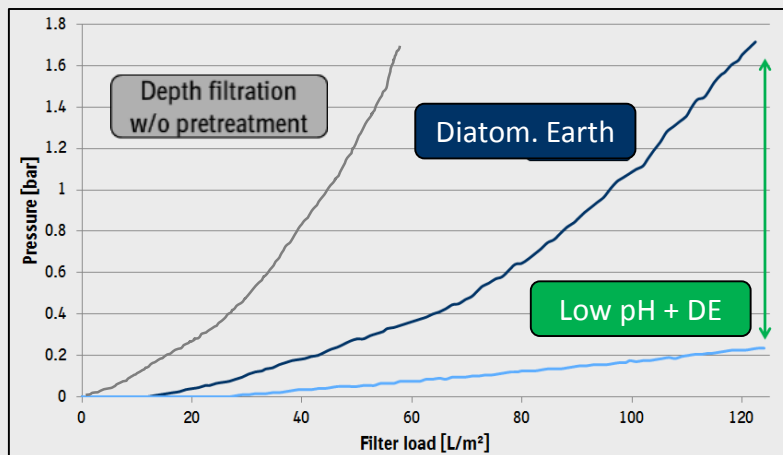
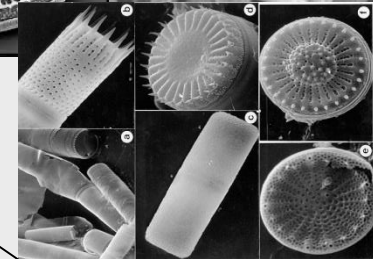
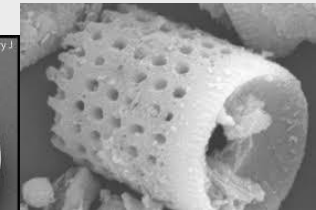
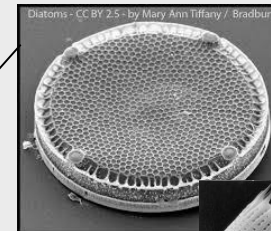
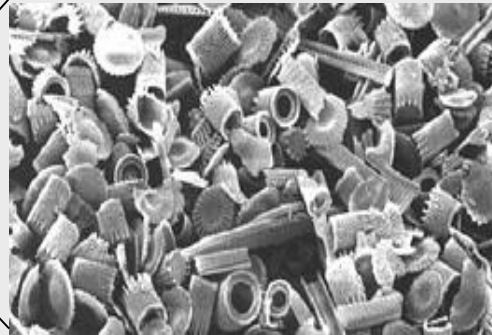
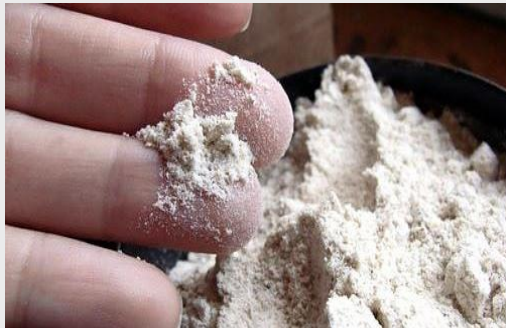
- Significant filter capacity increase by low pH precipitation processes
- Reduction of COGS for filtration



## Case Study III: Tech evaluation - Diatomaceous Earth Filtration

### Diatomaceous Earth Filtration:

- Established technology in food & beverage and pharmaceutical industry since decades
- Diatomaceous earth = inorganic, incompressible, inert and highly porous filter aid



- D.E.-Filtration: Proof-of-Concept studies in 2016 /17
- Lab scale experiments performed up to 80L scale
- Easy handling, good scalability
- High performance in combination with acid precipitation
- A real alternative for future SUB harvest processes !



# Cell Culture Harvest Development at BI

## Final Facts

- Boehringer Ingelheim BioXcellence® offers a high level of expertise in cell culture and harvest process development, scale up and process transfer of clinical trial or manufacturing processes for customers world-wide.
- BI's large network with global suppliers for separation and filtration technologies ensures the usage of state-of-the-art equipment and technology.
- Boehringer Ingelheim is continuously working on the evaluation of new cell culture harvest strategies like low pH precipitation, flocculation or diatomaceous earth filtration.
- Boehringer Ingelheim BioXcellence® offers a high degree of know how and expertise to develop processes from 500L – 2.000L SUB and up to 12.000L stainless steel production.

Thank you for your  
attention.

